

STUDY ON THE LN₂ CONSUMPTION OF THE BEAMLINE LN₂ TRANSFER SYSTEM FOR TPS PROJECT

H. C. Li, F. Z. Hsiao, H. H. Tsai, T. F. Lin, W. S. Chiou, S. H. Chang, W. R. Liao and W. S. Chan,
National Synchrotron Radiation Research Center, Hsinchu, 30076, Taiwan

Abstract

One system to transfer liquid nitrogen (LN₂) will be installed at TPS in 2015 for beamline. This system includes two transfer lines (length 600 m), eight keep-full devices and 26 branch lines with 26 control valves for 24 straight sections of beam lines. The required consumption of LN₂ for each beam line is 30 L/h. An archive system was developed to monitor and to calculate the consumption of LN₂ for each beam line. This consumption was calculated based on the pressure difference and the flow coefficient (K_v) of the control valve. This paper presents the configuration of the LN₂ supply system at NSRRC and a test bench of the calculation of LN₂ consumption. A simple test result is presented and discussed.

INTRODUCTION

A helium-cryogenic system with refrigeration (450 W) began its operation from 2003. The liquid-nitrogen (LN₂) supply system entered service at the same time. Figure 1 is the current status of the LN₂ supply system at NSRRC. The LN₂ supply system was finished for Taiwan Light Source (TLS) in 2009. The LN₂ transfer system for the Taiwan Photo Source (TPS) project began its installation and commissioning in 2013.

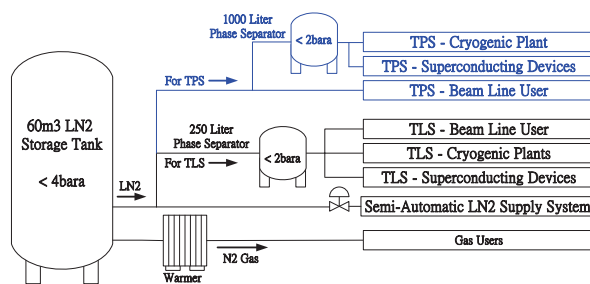


Figure 1: Configuration of the LN₂ supply system at NSRRC.

LN₂ Supply System at NSRRC

One LN₂ storage tank (60 m³) replaced the original one (20 m³) in 2009. In total, the LN₂ flows through a vacuum-shielded LN₂ transfer line (length > 300 m) and one phase separator (250 L) to users at TLS [1]. The TLS users comprised of two liquid-helium (LHe) refrigerators (450 W) [2], one superconducting RF cavity, five superconducting magnets, two beam-line laboratories, and one semi-automatic LN₂ supply system. A line (length >

300 m) for gaseous nitrogen (GN₂) used to purge or to clean the machine or experimental samples also existed inside the LN₂ system.

We installed a vacuum-shielded LN₂ transfer line (150 m), one phase separator (1000 L) and one helium refrigeration system (700 W) [3] in 2013. We finished the commissioning of a multi-channel line (LHe/GHe/LN₂/GN₂) for four TPS superconducting RF cavities in 2015 April. The total length is more than 130 m. We began to install two vacuum-shielded LN₂ transfer lines (length 600 m) with 26 control valves used in TPS beam-line laboratories in 2015 April. Figure 3 shows the configuration of the LN₂ transfer system of NSRRC.

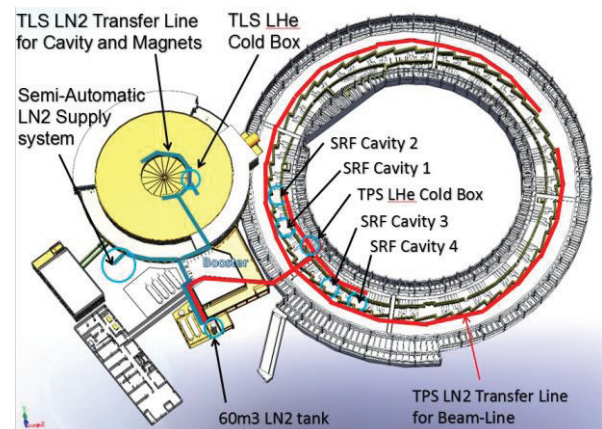


Figure 2: Configuration of LN₂ transfer line of NSRRC.

LN₂ Consumption

Increasing numbers of users introduce a rapidly increasing consumption of LN₂. Figure 3 shows the LN₂ consumption at NSRRC from 2005 to 2014. The average consumption is about 955 m³ per year from 2005 to 2009, but the average consumption increased to 1777 m³ per year from 2010 to 2014. The major increase was due to the TPS project. Many machines and systems were tested and commissioned during these five years. Figures 4 and 5 show the LN₂ ratio of users. It was easy to estimate the budget of TLS LN₂ consumption because of the stabilized operation in year 2009, but more than 51 % of the total amount LN₂ consumption was used to support the relevant testing of TPS in year 2013. It is difficult to estimate the LN₂ consumption under such conditions. To understand the LN₂ consumption of each user is an important issue for the stability of the LN₂ supply due to the budget control. A typical theory of valve sizing can help us to calculate the real-time consumption of LN₂

based on the pressure difference and the flow coefficient (K_v) of the control valve.

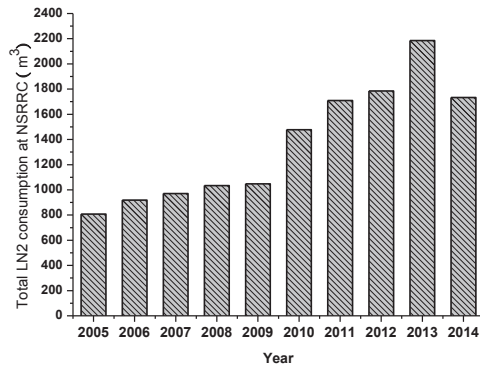


Figure 3: 10-year LN₂ consumption at NSRRC.

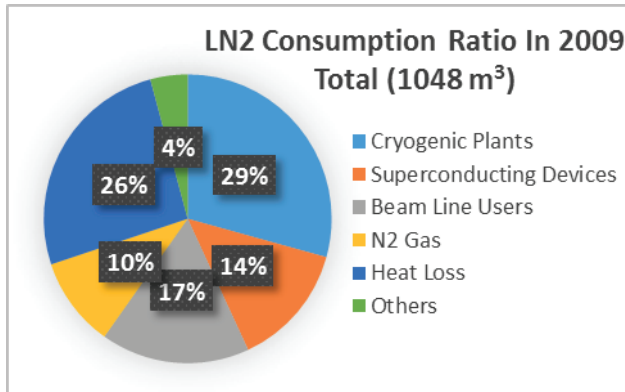


Figure 4: LN₂ consumption ratio in 2009.

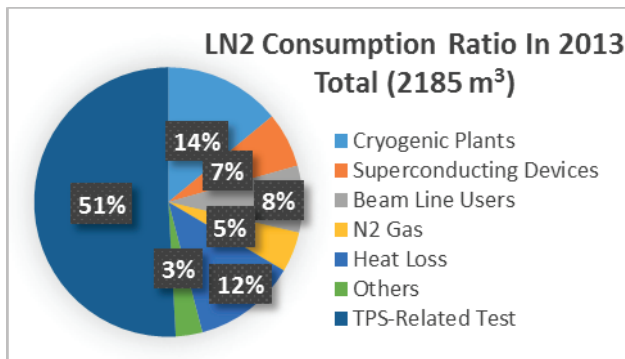


Figure 5: LN₂ consumption ratio in 2013.

LN₂ TRANSFER SYSTEM FOR THE TPS BEAM LINE

One system to transfer liquid nitrogen (LN₂) transfer system will be installed for the TPS beam line in 2015. This system includes two transfer lines (length 600 m), eight keep-full devices and 26 branch lines with 26 control valves for 24 straight sections of the beam line. The required consumption of LN₂ for each beam line is 30 L/h. One special design was implemented for a mass

flow-rate calculation of LN₂. Two pressure transducers are located upstream and downstream of each control valve, respectively, shown in Figure 6.

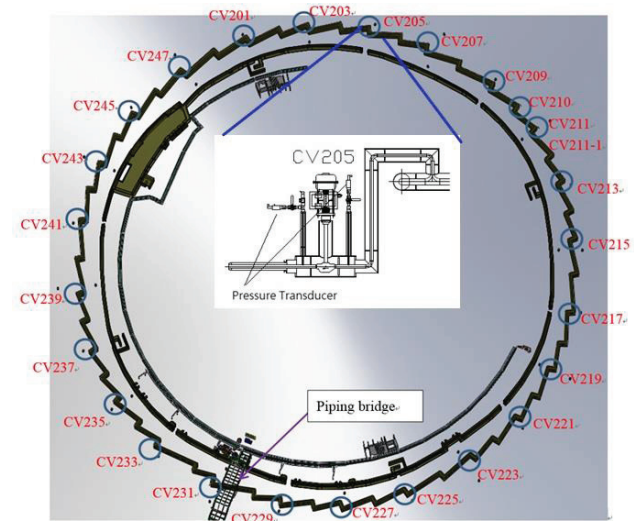


Figure 6: Overall transfer line for beam-line at TPS.

LN₂ Consumption Calculate

Three flow characteristics of a control valve are equal percentage, modified equal percentage and linear. The K_v (flow coefficient) value increases by the same increment for each fraction of travel of a control valve with ideal linear flow characteristics. In our LN₂ supply for the TPS beam line, we use a linear control valve to calculate easily the K_v value. A calculation of the K_v -value is standardized in IEC534 [4], but in our case the K_v -value was constant, as the control valve was chosen. We can then modify the formulae. Figure 7 shows a typical installation of a control valve in a control loop.

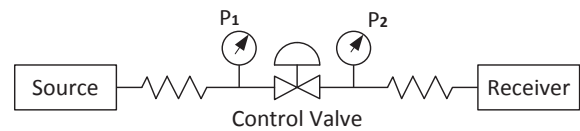


Figure 7: Typical installation of a control valve.

Of five equations to calculate the flow consumption with varied working fluids and flow conditions, equation (1) is used to calculate the liquid flow, equations (2) and (3) are used to calculate the gas flow, and equations (4) and (5) are used to calculate the vapour or steam.

$$W = K_v * \sqrt{1000 * \rho * \Delta p} \quad (1)$$

$$W = K_v * 519 * \sqrt{\frac{\rho_G * \Delta p * p_2}{T_1}} \quad (2)$$

$$\text{When } p_2 > p_1/2 \text{ and } \Delta p < p_1/2$$

$$W = K_v * 259.5 * P_1 * \sqrt{\frac{\rho_G}{T_1}} \quad (3)$$

When $p_2 < p_1/2$ and $\Delta p > p_1/2$

$$W = K_v * \sqrt{1000} * \sqrt{\frac{\Delta p}{v_2}} \quad (4)$$

When $p_2 > p_1/2$ and $\Delta p < p_1/2$

$$W = K_v * \sqrt{1000} * \sqrt{\frac{p_1}{2 * v^*}} \quad (5)$$

When $p_2 < p_1/2$ and $\Delta p > p_1/2$

The K_v value is here provided by a determined control valve. W (kg/h), p_1 (bar absolute) and p_2 (bar absolute) represent the fluid flow, the upstream pressure and the downstream pressure, respectively. Δp (bar) represents the pressure drop. ρ and ρ_G (kg/m³) represent the specific densities of gases at 273 K and 1.013 bar, T_1 (K) represents the upstream temperature. v_1 represents the specific volume of steam or vapour at p_1 and T_1 . v^* represents the specific volume of steam or vapour at $p_1/2$ and T_1 .

Test Bench and Test Result

On April 2015 we set up one simple test bench for the LN₂ consumption with varied K_v values of the control valve. The test bench comprised one control valve, two pressure transducers (PT), one LN₂ dewar, one scale and one gaseous-nitrogen mass-flow meter. Figure 9 shows the test bench for LN₂ consumption and measurement. A 20 % static opening was set for the control valve to perform the test. The calculated rate of mass flow was 2.41 kg/min based on equation (2), as the flow condition was closed two-phase flow. From the accessible data from the scale and the mass-flow meter we obtained a real number about 1.8 kg/min. There is a 25 % difference between the calculation and the measurement results.

The LN₂ transfer line is always a two-phase (LN₂ and GN₂) flow condition under normal operation. There is no

standard formula for two-phase flow. The described methods include much uncertainty. It is recommended that each separate calculation of the K_v -value of a liquid should add a factor. We shall try to find an appropriate factor for our system in the future.

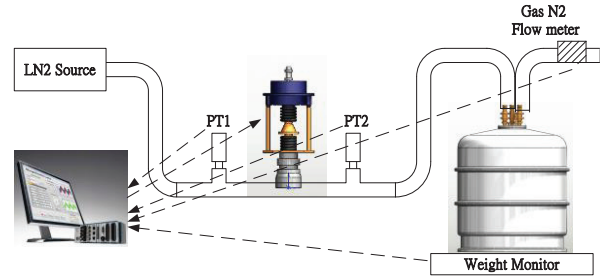


Figure 8: Test bench.

SUMMARY

The consumption of LN₂ at NSRRC increases annually because of the TPS project. In this work we tried to obtain the flow of LN₂ calculated based on the pressure difference and the flow coefficient (K_v) value of the control valve. We built a test bench to test the method and obtained an acceptable result. A preliminary test was performed, but we must implement one factor for every single branch line to have a precise formula to calculate the flow consumption that is near the real situation.

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