

# STUDY ON THE LN<sub>2</sub> CONSUMPTION OF THE BEAMLINE LN<sub>2</sub> TRANSFER SYSTEM FOR TPS PROJECT

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## Abstract

One system to transfer liquid nitrogen (LN<sub>2</sub>) will be installed at TPS in 2015 for beamline. This system includes two transfer lines (length 600 m), eight keep-full devices and 26 branch lines with 26 control valves for 24 straight sections of beam lines. The required consumption of LN<sub>2</sub> for each beam line is 30 L/h. An archive system was developed to monitor and to calculate the consumption of LN<sub>2</sub> for each beam line. This consumption was calculated based on the pressure difference and the flow coefficient ( $K_v$ ) of the control valve. This paper presents the configuration of the LN<sub>2</sub> supply system at NSRRC and a test bench of the calculation of LN<sub>2</sub> consumption. A simple test result is presented and discussed.

## INTRODUCTION

A helium-cryogenic system with refrigeration (450 W) began its operation from 2003. The liquid-nitrogen (LN<sub>2</sub>) supply system entered service at the same time. Figure 1 is the current status of the LN<sub>2</sub> supply system at NSRRC. The LN<sub>2</sub> supply system was finished for Taiwan Light Source (TLS) in 2009. The LN<sub>2</sub> transfer system for the Taiwan Photo Source (TPS) project began its installation and commissioning in 2013.

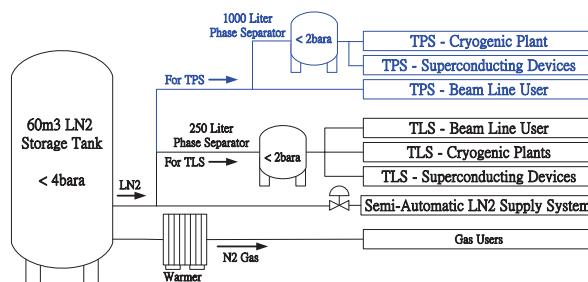


Figure 1: Configuration of the LN<sub>2</sub> supply system at NSRRC.

## LN<sub>2</sub> Supply System at NSRRC

One LN<sub>2</sub> storage tank (60 m<sup>3</sup>) replaced the original one (20 m<sup>3</sup>) in 2009. In total, the LN<sub>2</sub> flows through a vacuum-shielded LN<sub>2</sub> transfer line (length > 300 m) and one phase separator (250 L) to users at TLS [1]. The TLS users comprised of two liquid-helium (LHe) refrigerators (450 W) [2], one superconducting RF cavity, five superconducting magnets, two beam-line laboratories, and one semi-automatic LN<sub>2</sub> supply system. A line (length >

300 m) for gaseous nitrogen (GN<sub>2</sub>) used to purge or to clean the machine or experimental samples also existed inside the LN<sub>2</sub> system.

We installed a vacuum-shielded LN<sub>2</sub> transfer line (150 m), one phase separator (1000 L) and one helium refrigeration system (700 W) [3] in 2013. We finished the commissioning of a multi-channel line (LHe/GHe/LN<sub>2</sub>/GN<sub>2</sub>) for four TPS superconducting RF cavities in 2015 April. The total length is more than 130 m. We began to install two vacuum-shielded LN<sub>2</sub> transfer lines (length 600 m) with 26 control valves used in TPS beam-line laboratories in 2015 April. Figure 3 shows the configuration of the LN<sub>2</sub> transfer system of NSRRC.

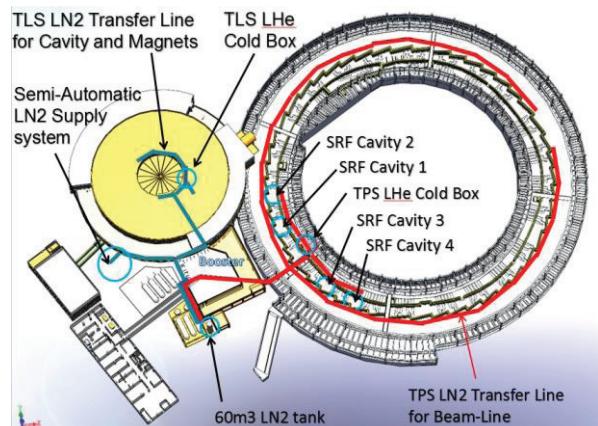


Figure 2: Configuration of LN<sub>2</sub> transfer line of NSRRC.

## LN<sub>2</sub> Consumption

Increasing numbers of users introduce a rapidly increasing consumption of LN<sub>2</sub>. Figure 3 shows the LN<sub>2</sub> consumption at NSRRC from 2005 to 2014. The average consumption is about 955 m<sup>3</sup> per year from 2005 to 2009, but the average consumption increased to 1777 m<sup>3</sup> per year from 2010 to 2014. The major increase was due to the TPS project. Many machines and systems were tested and commissioned during these five years. Figures 4 and 5 show the LN<sub>2</sub> ratio of users. It was easy to estimate the budget of TLS LN<sub>2</sub> consumption because of the stabilized operation in year 2009, but more than 51 % of the total amount LN<sub>2</sub> consumption was used to support the relevant testing of TPS in year 2013. It is difficult to estimate the LN<sub>2</sub> consumption under such conditions. To understand the LN<sub>2</sub> consumption of each user is an important issue for the stability of the LN<sub>2</sub> supply due to the budget control. A typical theory of valve sizing can help us to calculate the real-time consumption of LN<sub>2</sub>.

based on the pressure difference and the flow coefficient ( $K_v$ ) of the control valve.

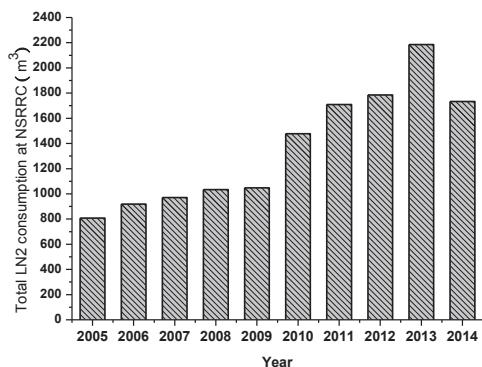


Figure 3: 10-year LN<sub>2</sub> consumption at NSRRC.

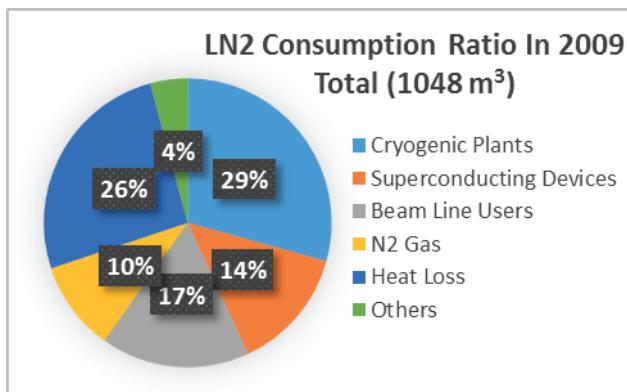


Figure 4: LN<sub>2</sub> consumption ratio in 2009.

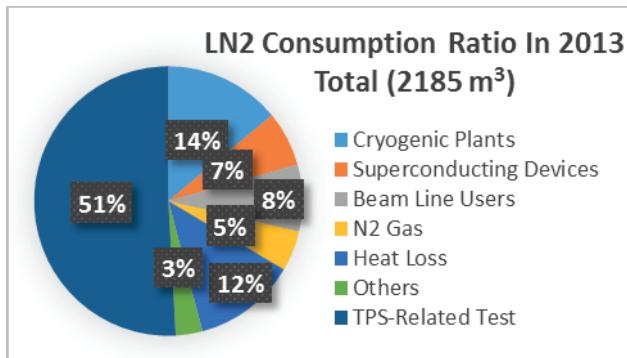


Figure 5: LN<sub>2</sub> consumption ratio in 2013.

## LN<sub>2</sub> TRANSFER SYSTEM FOR THE TPS BEAM LINE

One system to transfer liquid nitrogen (LN<sub>2</sub>) transfer system will be installed for the TPS beam line in 2015. This system includes two transfer lines (length 600 m), eight keep-full devices and 26 branch lines with 26 control valves for 24 straight sections of the beam line. The required consumption of LN<sub>2</sub> for each beam line is 30 L/h. One special design was implemented for a mass

flow-rate calculation of LN<sub>2</sub>. Two pressure transducers are located upstream and downstream of each control valve, respectively, shown in Figure 6.

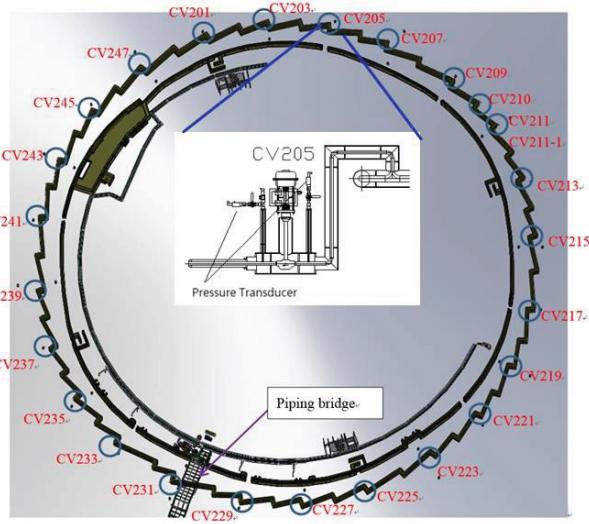


Figure 6: Overall transfer line for beam-line at TPS.

### LN<sub>2</sub> Consumption Calculate

Three flow characteristics of a control valve are equal percentage, modified equal percentage and linear. The  $K_v$  (flow coefficient) value increases by the same increment for each fraction of travel of a control valve with ideal linear flow characteristics. In our LN<sub>2</sub> supply for the TPS beam line, we use a linear control valve to calculate easily the  $K_v$  value. A calculation of the  $K_v$ -value is standardized in IEC534 [4], but in our case the  $K_v$ -value was constant, as the control valve was chosen. We can then modify the formulae. Figure 7 shows a typical installation of a control valve in a control loop.

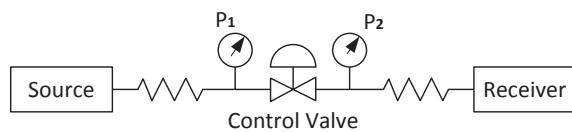


Figure 7: Typical installation of a control valve.

Of five equations to calculate the flow consumption with varied working fluids and flow conditions, equation (1) is used to calculate the liquid flow, equations (2) and (3) are used to calculate the gas flow, and equations (4) and (5) are used to calculate the vapour or steam.

$$W = K_v * \sqrt{1000 * \rho * \Delta p} \quad (1)$$

$$W = K_v * 519 * \sqrt{\frac{\rho_g * \Delta p * p_2}{T_1}} \quad (2)$$

When  $p_2 > p_1/2$  and  $\Delta p < p_1/2$

$$W = Kv * 259.5 * P_1 * \sqrt{\frac{\rho_G}{T_1}} \quad (3)$$

When  $p_2 < p_1/2$  and  $\Delta p > p_1/2$

$$W = Kv * \sqrt{1000} * \sqrt{\frac{\Delta p}{v_2}} \quad (4)$$

When  $p_2 > p_1/2$  and  $\Delta p < p_1/2$

$$W = Kv * \sqrt{1000} * \sqrt{\frac{p_1}{2 * v^*}} \quad (5)$$

When  $p_2 < p_1/2$  and  $\Delta p > p_1/2$

The  $K_v$  value is here provided by a determined control valve.  $W$  (kg/h),  $p_1$  (bar absolute) and  $p_2$  (bar absolute) represent the fluid flow, the upstream pressure and the downstream pressure, respectively.  $\Delta p$  (bar) represents the pressure drop.  $\rho$  and  $\rho_G$  (kg/m<sup>3</sup>) represent the specific densities of gases at 273 K and 1.013 bar,  $T_1$  (K) represents the upstream temperature.  $v_1$  represents the specific volume of steam or vapour at  $p_1$  and  $T_1$ .  $v^*$  represents the specific volume of steam or vapour at  $p_1/2$  and  $T_1$ .

### Test Bench and Test Result

On April 2015 we set up one simple test bench for the LN<sub>2</sub> consumption with varied  $K_v$  values of the control valve. The test bench comprised one control valve, two pressure transducers (PT), one LN<sub>2</sub> dewar, one scale and one gaseous-nitrogen mass-flow meter. Figure 9 shows the test bench for LN<sub>2</sub> consumption and measurement. A 20 % static opening was set for the control valve to perform the test. The calculated rate of mass flow was 2.41 kg/min based on equation (2), as the flow condition was closed two-phase flow. From the accessible data from the scale and the mass-flow meter we obtained a real number about 1.8 kg/min. There is a 25 % difference between the calculation and the measurement results.

The LN<sub>2</sub> transfer line is always a two-phase (LN<sub>2</sub> and GN<sub>2</sub>) flow condition under normal operation. There is no

standard formula for two-phase flow. The described methods include much uncertainty. It is recommended that each separate calculation of the  $K_v$ -value of a liquid should add a factor. We shall try to find an appropriate factor for our system in the future.

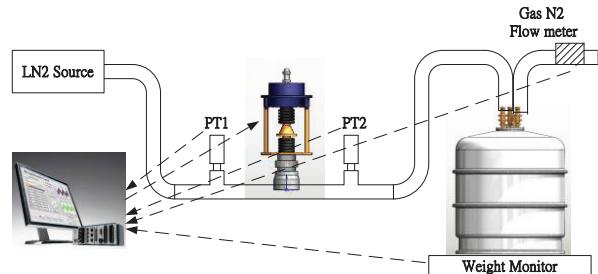


Figure 8: Test bench.

### SUMMARY

The consumption of LN<sub>2</sub> at NSRRC increases annually because of the TPS project. In this work we tried to obtain the flow of LN<sub>2</sub> calculated based on the pressure difference and the flow coefficient ( $K_v$ ) value of the control valve. We built a test bench to test the method and obtained an acceptable result. A preliminary test was performed, but we must implement one factor for every single branch line to have a precise formula to calculate the flow consumption that is near the real situation.

### REFERENCES

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- [4] WEKA Specification no. 20080118 "Calculation of Valve Kv-Value - Inherent Rangeability - Flow Characteristics"